

# The *stoich* module

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*Note: this is the stoich.ipynb notebook. The PDF version "The stoich module" is available [here](#).*

## 1 Introduction

**BondGraphTools** is a python based toolkit for the creation and analysis of bond graph models of physical systems. Such physical systems include biomolecular systems; **stoich** is a toolkit for the stoichiometric analysis of such systems.

This document provides a simple introduction to **stoich** by means of a built-in bond graph model of a simple enzyme-catalysed reaction.

## 2 Example.

**stoich.model()** implements the enzyme-catalysed reaction:  $A+E = C = B+E$  where A is the substrate, B the product, E the enzyme and C an intermediate compound. This can be analysed using the following code.

First import some code:

```
In [1]: import BondGraphTools as bgt
import numpy as np
import sympy as sp
import IPython.display as disp
import stoich as st
```

### 2.1 Basic analysis

Now perform stoichiometric analysis on the model:

```
In [2]: s = st.stoich(st.model())
```

```
Swapping Re:r1 for two Sf in ABCE
Swapping Re:r2 for two Sf in ABCE
```

s is a Python dict containing the stoichiometric information. For example, the stoichiometric matrix  $N$  where  $\dot{X} = NV$  is revealed as:

```
In [3]: print(s['N'])
```

```
[[-1  0]
 [ 0  1]
 [ 1 -1]
 [-1  1]]
```

This can be displayed in a more readable form as:

```
In [4]: disp.Latex(st.sprint1(s, 'N'))
```

Out [4] :

$$N = \begin{pmatrix} -1 & 0 \\ 0 & 1 \\ 1 & -1 \\ -1 & 1 \end{pmatrix} \quad (1)$$

The state (vector of concentrations)  $X$  and the vector  $V$  of reaction flows are:

In [5] : `disp.Latex(st.sprintl(s, 'species'))`

Out [5] :

$$X = \begin{pmatrix} X_A \\ X_B \\ X_C \\ X_E \end{pmatrix} \quad (2)$$

In [6] : `disp.Latex(st.sprintl(s, 'reaction'))`

Out [6] :

$$V = \begin{pmatrix} V_{r1} \\ V_{r2} \end{pmatrix} \quad (3)$$

The corresponding reactions can be displayed:

In [7] : `disp.Latex(st.sprintrl(s))`

Out [7] :



The stoichiometric matrix  $N$  gives the species state  $X$  in terms of reaction flow  $V$  from  $\dot{X} = NV$ .  $N$  is also used together with thermodynamic constants  $K$  and rate constants  $\kappa$  to give an explicit expression for reaction flow  $V$  in terms of species state  $X$ . `stoich` computes the symbolic expression as:

In [8] : `disp.Latex(st.sprintl(s, 'N'))`

Out [8] :

$$N = \begin{pmatrix} -1 & 0 \\ 0 & 1 \\ 1 & -1 \\ -1 & 1 \end{pmatrix} \quad (6)$$

```
In [9]: disp.Latex(st.sprintv1(s))
```

```
Out [9]:
```

$$v_{r1} = \kappa_{r1} (K_A K_E x_A x_E - K_C x_C) \quad (7)$$

$$v_{r2} = \kappa_{r2} (-K_B K_E x_B x_E + K_C x_C) \quad (8)$$

## 2.2 Conserved moieties and Pathways

Conserved moieties are revealed by the matrix  $G$  where  $G^T N = 0$ . In this case:

```
In [10]: disp.Latex(st.sprint1(s, 'G'))
```

```
Out [10]:
```

$$G = \begin{pmatrix} 1 & 1 & 1 & 0 \\ -1 & -1 & 0 & 1 \end{pmatrix} \quad (9)$$

The first row corresponds to  $\dot{x}_A + \dot{x}_B + \dot{x}_C = 0$ , the sum of the rows (0 0 1 1) corresponds to  $\dot{x}_C + \dot{x}_E = 0$

Pathways are revealed by the matrix  $K$  where  $NK = 0$ . In this case:

```
In [11]: disp.Latex(st.sprint1(s, 'K'))
```

```
Out [11]:
```

$$K \Rightarrow () \quad (10)$$

There are no pathways: there is zero flow ( $V = 0$ ) in the steady state.

## 2.3 Chemostats.

Consider the case where both substrate  $A$  and product  $B$  are chemostats:

```
In [12]: chemostats = ['A', 'B']
```

The same system, but with the chemostats, can be analysed using:

```
In [13]: sc = st.statify(s, chemostats=chemostats)
```

The stoichiometric matrix  $N$  is now:

```
In [14]: disp.Latex(st.sprint1(sc, 'N'))
```

Out [14]:

$$N = \begin{pmatrix} 0 & 0 \\ 0 & 0 \\ 1 & -1 \\ -1 & 1 \end{pmatrix} \quad (11)$$

The first two rows are zero, corresponding to  $\dot{x}_A = \dot{x}_B = 0$ : this is because both substrate  $A$  and product  $B$  are chemostats.

The pathway matrix  $K$  is now:

In [15]: `disp.Latex(st.sprintl(sc, 'K'))`

Out [15]:

$$K = \begin{pmatrix} 1 \\ 1 \end{pmatrix} \quad (12)$$

This means that the flow through reactions  $r1$  and  $r2$  are the same and can be non-zero at steady-state. The conserved moieties of this chemostated system are revealed by the matrix  $G$

In [16]: `disp.Latex(st.sprintl(sc, 'G'))`

Out [16]:

$$G = \begin{pmatrix} 1 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 1 & 1 \end{pmatrix} \quad (13)$$

The three rows correspond to:  $-\dot{x}_A = 0$  ( $x_A$  is constant) -  $\dot{x}_B = 0$  ( $x_B$  is constant) -  $\dot{x}_C + \dot{x}_E = 0$  ( $x_C + x_E$  is constant)

## 2.4 Pathway analysis

In [17]: `## Find the pathway stoichiometric matrix`  
`sp = st.path(s,sc)`  
`## And show the coreponding reaction`  
`disp.Latex(st.sprintrl(sp))`

Out [17]:



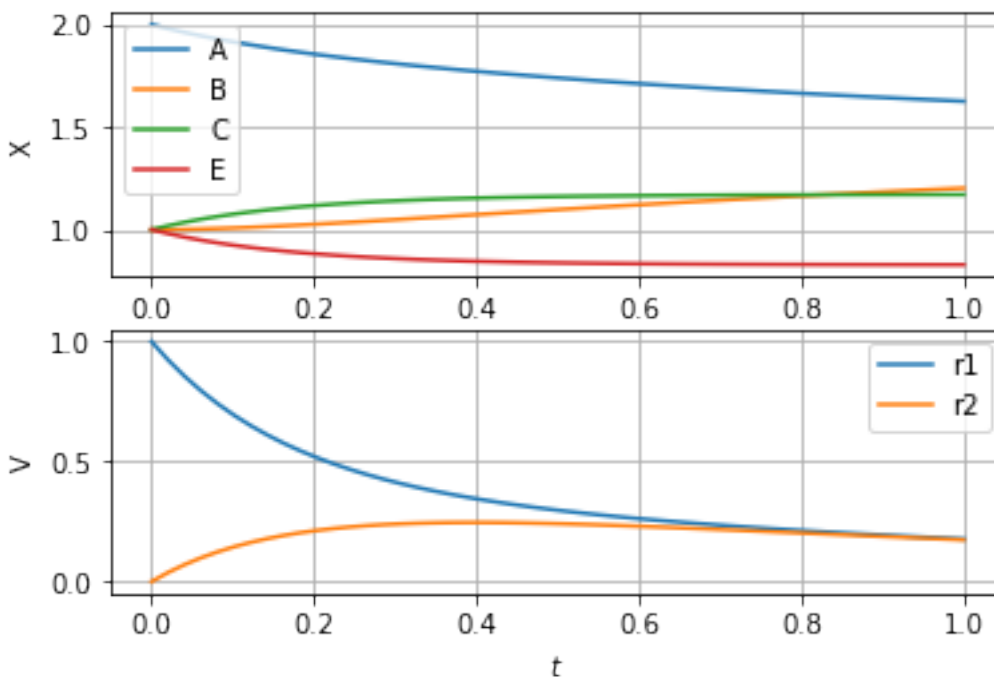
## 2.5 Simulation

Although **BondGraphTools** has its own simulation tool, the particular form of stoichiometric equations allows for a special purpose simulation tool taking advantage of explicit equations and reducing the state dimension in the presence of conserved moieties.

The system (without chemostats) can be simulated as:

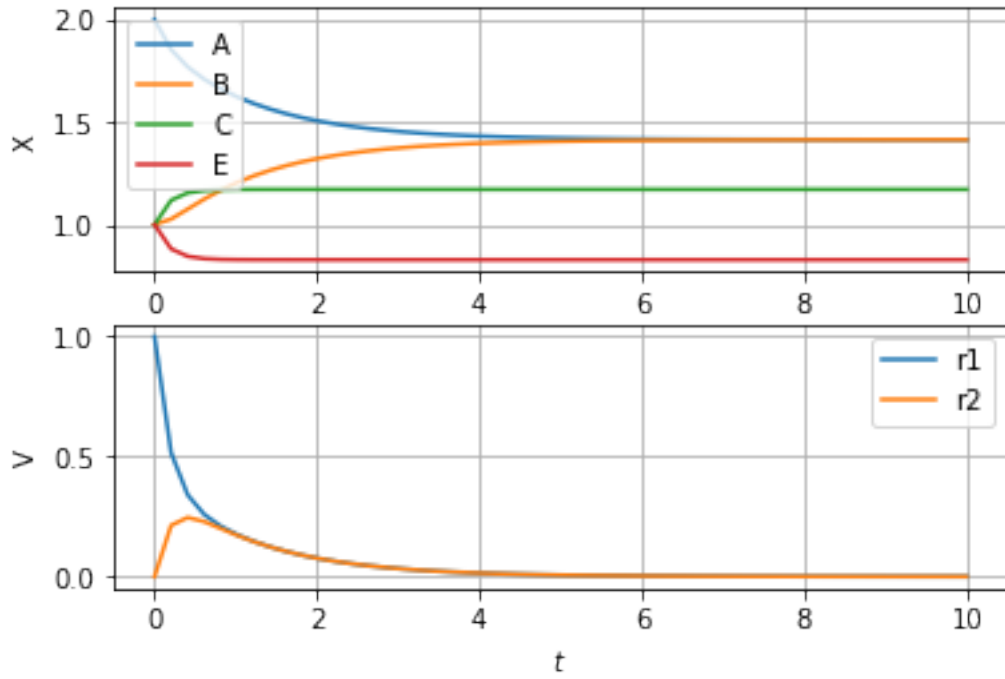
```
In [18]: X0 = np.array([2,1,1,1]) # Set initial states
         result = st.sim(s,X0=X0) # Simulate
```

```
In [19]: st.plot(s,result)
```



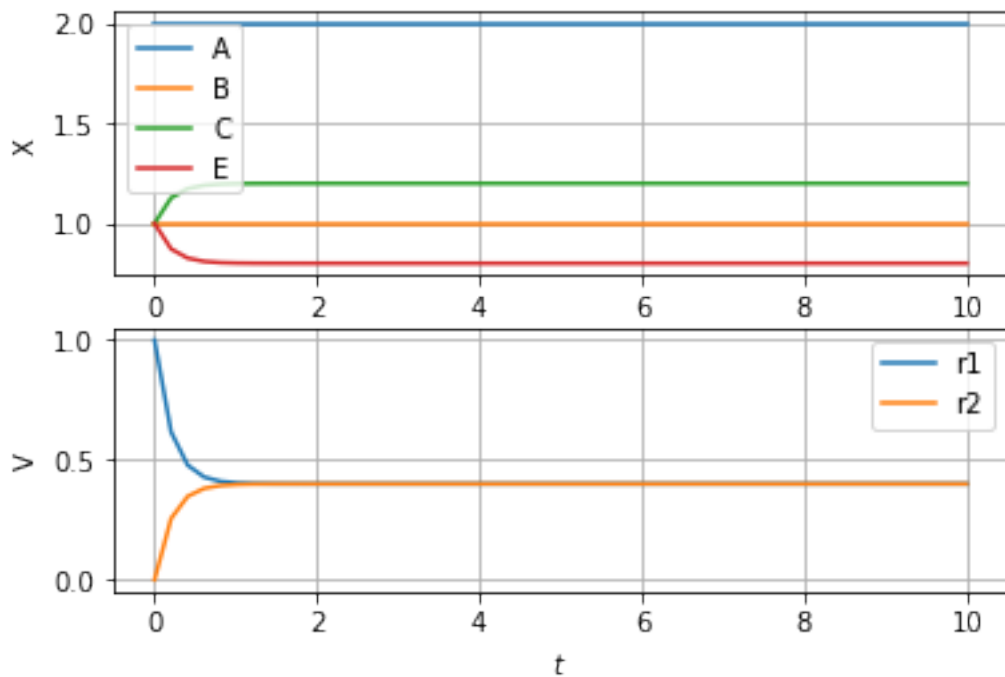
The flows  $V$  through  $r1$  and  $r2$  seem to be heading towards zero as predicted by pathway analysis. This can be verified by simulating over a longer time:

```
In [20]: t = np.linspace(0,10)
         result = st.sim(s,X0=X0,t=t)
         st.plot(s,result)
```



The system with chemostats can be simulated as:

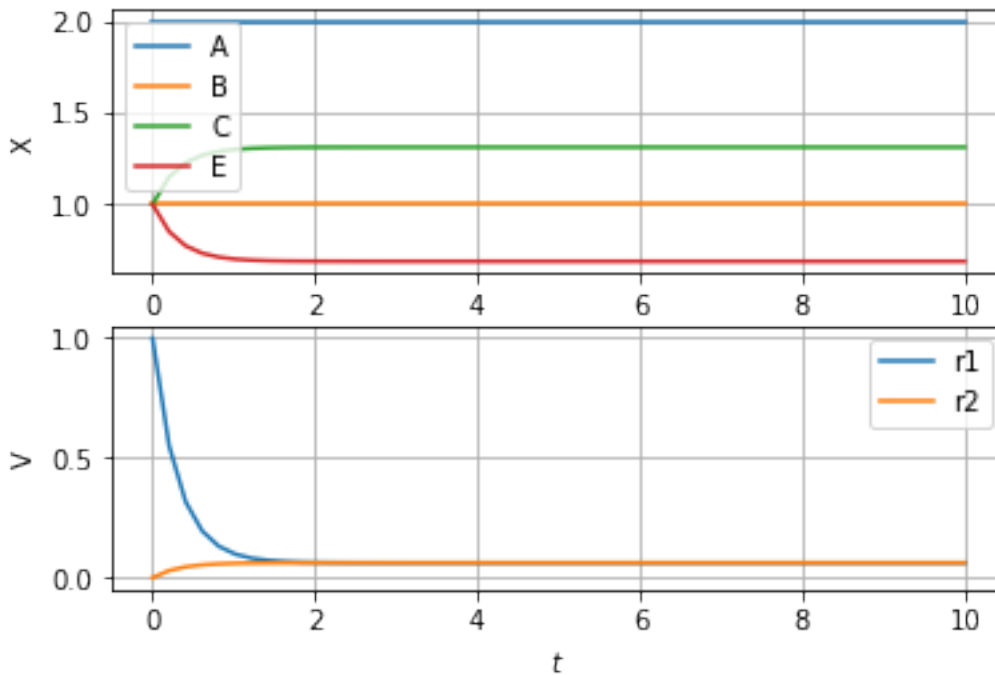
```
In [21]: t = np.linspace(0,10)
         result = st.sim(s,X0=X0,t=t,sc=sc)
         st.plot(s,result)
```



As predicted by pathway analysis, the two flows converge on a non-zero value.

Of course, these simulations have been using default (unity) values for parameters. These defaults can be changed by explicitly supplying parameters:

```
In [22]: parameter={'kappa_r2':0.1}
         result = st.sim(s,X0=X0,t=t,sc=sc,parameter=parameter)
         st.plot(s,result)
```



Moreover, the four initial conditions can be explicitly chosen, for example: -

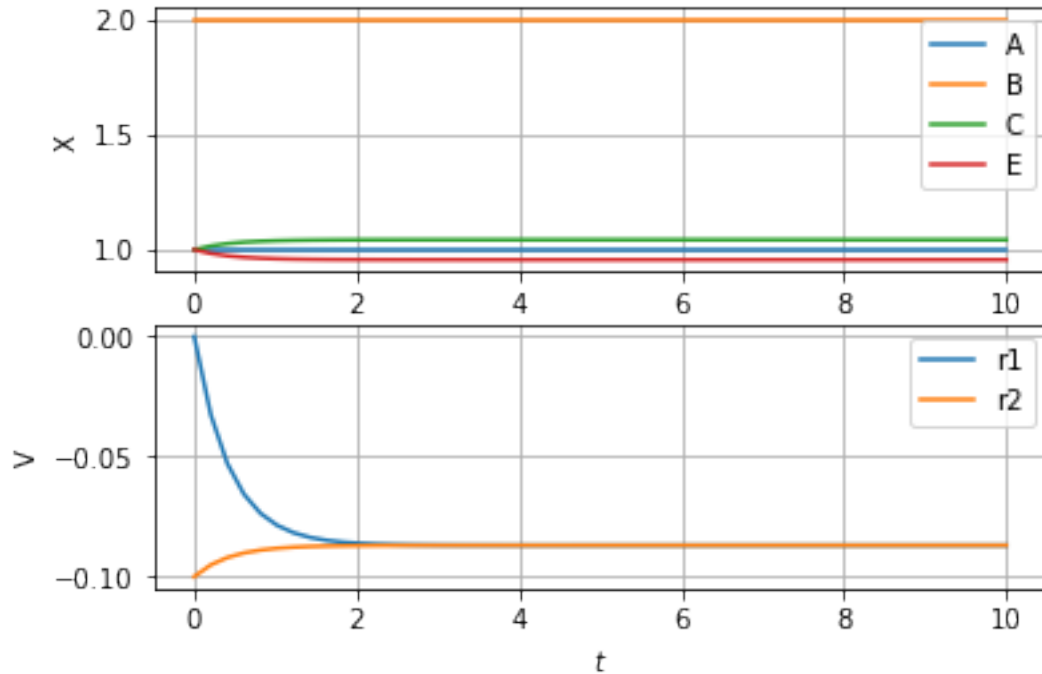
$$X_0 = (1 \ 2 \ 1 \ 1)^T$$

Note that the default value was -

$$X_0 = (2 \ 1 \ 1 \ 1)^T$$

```
In [23]: X0 = np.array([1,2,1,1])
         result = st.sim(s,t=t,sc=sc,parameter=parameter,X0=X0)
         st.plot(s,result)
```



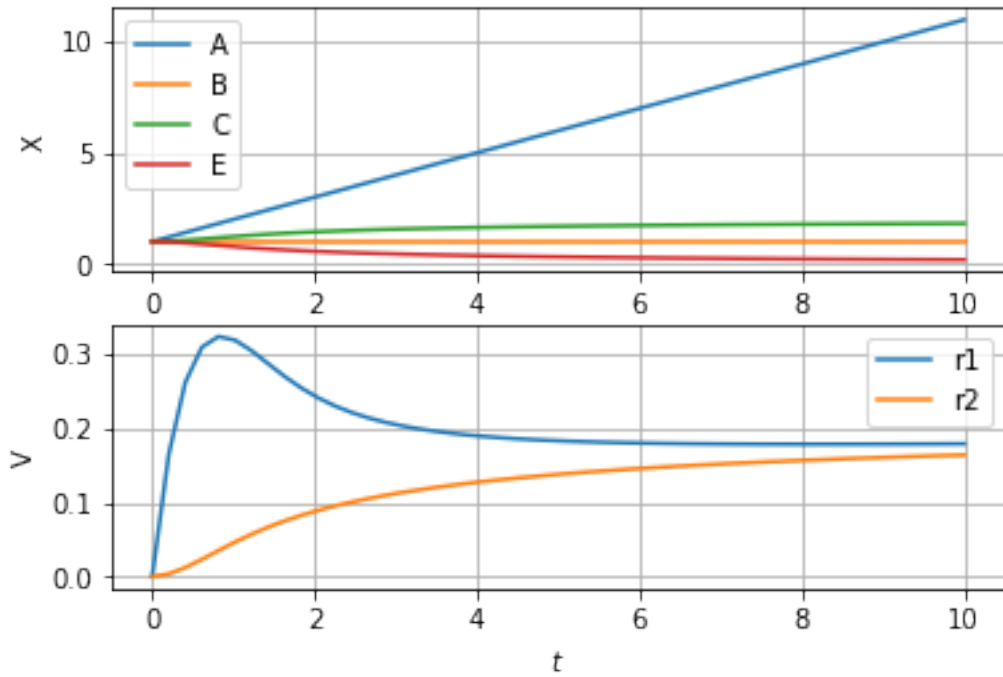


As the product  $B$  amount is greater than that of the substrate  $A$ , the flow proceeds in reverse.

### 2.5.1 Time-varying chemostats

By default, chemostats remain at the corresponding initial state. This can be changed by declaring a time-varying expression for the chemostat state. For example, set the chemostat for substrate  $A$  to have a value of  $1 + t$ :

```
In [24]: X_chemo = {'A': '1+t'}
         result = st.sim(s,t=t,sc=sc,parameter=parameter,X_chemo=X_chemo)
         st.plot(s,result)
```



Note that the flow rates reach a maximum value as the amount of enzyme  $x_E$  reduces to zero. This behaviour is typical of systems with conserved moities in general and enzyme catalysed reactions in particular.

## References